

# iemisc: Calculating the Friction Loss Examples

Irucka Embry, E.I.T. (EcoC<sup>2</sup>S)

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## Replicate the R code

Note: If you wish to replicate the R code below, then you will need to copy and paste the following commands in R first (to make sure you have all the packages and their dependencies):

```
install.packages(c("install.load", "iemisc", "data.table", "units", "pander", "pracma"))  
# install the packages and their dependencies
```

```
# load the required packages  
install.load::load_package("iemisc", "data.table", "units", "pander")  
# load needed packages using the load_package function from the install.load  
# package (it is assumed that you have already installed these packages)
```

```
import::from(pracma, newtonRaphson)  
# import newtonRaphson from the pracma package
```

## Example 1 Set – Example 17.2 (Lindeburg Manual Reference)

Please note that the f2, f3, f4, f5, f6, f7, f8, and the relerror functions are found within the iemisc R package created by Irucka Embry

Answers from the Lindeburg Manual Reference text:

0.028 - Moody diagram

0.0287 - Appendix 17.B “Darcy Friction Factors (turbulent flow)”

0.0288 - Swamee-Jain approximation

0.0287 - Colebrook equation

```
Re <- 4e+05
```

```
eps <- 0.004
```

```
D <- 1
```

```
eps/D
```

```
## [1] 0.004
```

```
f2 <- f2(eps = eps, D = D, Re = Re)
```

```
f2
```

```
## [1] 0.02944312
```

```
f3 <- f3(eps = eps, D = D, Re = Re)
```

```
f3
```

```
## [1] 0.0286854
```

```
f4 <- f4(eps = eps, D = D, Re = Re)
```

```
f4
```

```
## [1] 0.02867517
```

```
f5 <- f5(eps = eps, D = D, Re = Re)
```

```
f5
```

```
## [1] 0.02869798
```

```
f6 <- f6(eps = eps, D = D, Re = Re)
```

```
f6
```

```
## [1] 0.02881149
```

```
f7 <- f7(eps = eps, D = D, Re = Re)
```

```
f7
```

```
## [1] 0.02869798
```

```
f8 <- f8(eps = eps, D = D, Re = Re)
```

```
f8
```

```
## [1] 0.02867606
```

```
# determine the relative error
```

```
acc <- 0.0287
```

```
relerror(acc, f2)
```

```
## [1] 2.589255
```

```
releerror(acc, f3)
## [1] 0.05086994
releerror(acc, f4)
## [1] 0.08652119
releerror(acc, f5)
## [1] 0.00704152
releerror(acc, f6)
## [1] 0.3884771
releerror(acc, f7)
## [1] 0.007044366
releerror(acc, f8)
## [1] 0.08341057
```

## Example 2 Set – Example 2 (EngineerExcel Reference)

Please note that the f2, f3, f4, f5, f6, f7, and the f8 functions are found within the iemisc R package created by Irucka Embry

```
eps <- 5e-05
D <- 0.0254
Re <- 6000
# f equal to 0.0375 from Microsoft Excel Goal Seek
f2(eps = eps, D = D, Re = Re)
## [1] 0.0379846
f3(eps = eps, D = D, Re = Re)
## [1] 0.03555518
f4(eps = eps, D = D, Re = Re)
## [1] 0.03549632
f5(eps = eps, D = D, Re = Re)
## [1] 0.03781183
f6(eps = eps, D = D, Re = Re)
## [1] 0.03843287
```

```
f7(eps = eps, D = D, Re = Re)
## [1] 0.03549702
f8(eps = eps, D = D, Re = Re)
## [1] 0.03781382
```

## Problem 1 Statement

Example 1 [Kudela]

“Oil, with  $\rho = 900 \text{ kg/m}^3$  and kinematic coefficient of viscosity  $\nu = 0,00001 \text{ m}^2/\text{s}$ , flows at  $q_v = 0,2 \text{ m}^3/\text{s}$  through 500 m of 200-mm diameter cast-iron pipe. Determine the head loss.”

“Absolute roughness for iron-cast pipe is  $\epsilon = 0.26 \text{ mm}$ .”

## Solution 1 for the Problem 1 Statement

```
# Please note that the Re2, f2, f3, f4, f5, f6, f7, f8, and the colebrook
# functions are found within the iemisc R package created by Irucka Embry

# oil iron-cast pipe find the friction loss -- the head loss is 117 meters

# given the water flow of 0.2 m^3/s create a numeric vector with the units of
# cubic meters per second for the volumetric flow rate
Vdot <- set_units(0.2, m^3/s)
Vdot

## 0.2 [m^3/s]

# given length of 500 m create a numeric vector with the units of meters
L_SI <- set_units(500, m)
L_SI

## 500 [m]

g_SI <- set_units(9.80665, m/s^2)
g_SI

## 9.80665 [m/s^2]

# given saturated liquid density of oil (SI units)
rho_SI <- set_units(900, kg/m^3)
rho_SI

## 900 [kg/m^3]
```

```

# given kinematic viscosity of oil (SI units)
nu_SI <- set_units(1e-05, m^2/s)
nu_SI

## 1e-05 [m^2/s]
# create a numeric vector with the units of millimeters for the given specific
# roughness
epsilon <- set_units(0.26, mm)
epsilon

## 0.26 [mm]
# create a numeric vector with the units of meters for the given specific
# roughness
epsilon <- epsilon

units(epsilon) <- make_units(m)
epsilon

## 0.00026 [m]
# create a numeric vector with the units of millimeters for the given internal
# pipe diameter
Di <- set_units(200, mm)
Di

## 200 [mm]
# create a numeric vector with the units of meters for the given internal pipe
# diameter
units(Di) <- make_units(m)
Di

## 0.2 [m]
# relative roughness (dimensionless) of the cast iron pipe
rel_roughness <- epsilon/Di
rel_roughness

## 0.0013 [1]
# internal area of the cast iron pipe
Ai <- Di^2 * pi/4
Ai

## 0.03141593 [m^2]
# average velocity of the flowing water
V <- Vdot/Ai
V

## 6.366198 [m/s]
# Reynolds number using the kinematic viscosity
Re_SI <- Re2(D = drop_units(Di), V = drop_units(V), nu = drop_units(nu_SI))
Re_SI

## [1] 127324

```

```

# Darcy friction factor (f) for cast iron pipe Moody equation
fr2_SI <- f2(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI)

# Romeo, et. al. equation
fr3_SI <- f3(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI)

# Žarko Čojbašića and Dejan Brkić equation
fr4_SI <- f4(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI)

# Colebrook-White equation
fr5_SI <- f5(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI)

# Colebrook-White equation from Didier Clamond
colebrook_SI <- colebrook(Re_SI, K = drop_units(rel_roughness))

# Swamee-Jaine equation
fr6_SI <- f6(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI)

# Zigrang-Sylvester equation
fr7_SI <- f7(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI)

# Vatankhah equation
fr8_SI <- f8(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI)

# friction loss for cast iron pipe
hf_SI1 <- (f2(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI) * drop_units(L_SI) *
  drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_SI))

hf_SI2 <- (f3(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI) * drop_units(L_SI) *
  drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_SI))

hf_SI3 <- (f4(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI) * drop_units(L_SI) *
  drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_SI))

hf_SI4 <- (f5(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI) * drop_units(L_SI) *
  drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_SI))

hf_SI5 <- (colebrook(Re_SI, K = drop_units(rel_roughness)) * drop_units(L_SI) * drop_units(V)^2)/(2 *
  drop_units(Di) * drop_units(g_SI))

hf_SI6 <- (f6(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI) * drop_units(L_SI) *
  drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_SI))

hf_SI7 <- (f7(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI) * drop_units(L_SI) *
  drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_SI))

hf_SI8 <- (f8(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_SI) * drop_units(L_SI) *
  drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_SI))

# result table
result_table_SI <- data.table(V1 = c("Moody equation", "Romeo, et. al. equation",

```

```

"Žarko Čojbašića and Dejan Brkić equation", "Colebrook-White equation",
"Colebrook-White equation from Didier Clamond", "Swamee-Jaine equation", "Zigrang-Sylvester equation",
"Vatankhah equation"), V2 = c(fr2_SI, fr3_SI, fr4_SI, fr5_SI, colebrook_SI, fr6_SI,
fr7_SI, fr8_SI), V3 = c(hf_SI1, hf_SI2, hf_SI3, hf_SI4, hf_SI5, hf_SI6, hf_SI7,
hf_SI8))

setnames(result_table_SI, c("Darcy friction factor equation", "Darcy friction factor (f) for cast iron pipe",
"Friction loss for cast iron pipe over total length"))

pander(result_table_SI)

```

Darcy friction factor equation	Darcy friction factor (f) for cast iron pipe
Moody equation	0.02329
Romeo, et. al. equation	0.01745
Žarko Čojbašića and Dejan Brkić equation	0.01743
Colebrook-White equation	0.02272
Colebrook-White equation from Didier Clamond	0.01711
Swamee-Jaine equation	0.02291
Zigrang-Sylvester equation	0.01742
Vatankhah equation	0.02271

Friction loss for cast iron pipe over total length
120.3
90.14
90.05
117.4
88.41
118.4
89.98
117.3

Henryk Kudela calculated 117 meters for the head loss.

## Problem 2 Statement

Example 1 [Subramanian]

Find the head loss due to the flow of 1,500 gpm of oil ( $\nu = 1.15 \times 10^{-4}$  ft<sup>2</sup>/s) through 1,600 feet of 8" diameter cast iron pipe. The density of the oil  $\rho = 1.75$  slug/ft<sup>3</sup>.

“For cast iron,  $\epsilon = 8.5 \times 10^{-4}$  ft.”

## Solution 2 for the Problem 2 Statement

```
# Please note that the Re2, f2, f3, f4, f5, f6, f7, f8, and the colebrook
# functions are found within the iemisc R package created by Irucka Embry

# oil cast iron pipe find the head loss -- the head loss is 83.7 feet

# given the water flow of 1500 gpm (gal / min) create a numeric vector with the
# units of gallons per minute for the volumetric flow rate
Vdot <- set_units(1500, gallon/min)
Vdot

## 1500 [gallon/min]
# create a numeric vector with the units of cubic feet per second for the
# volumetric flow rate
units(Vdot) <- make_units(ft^3/sec)
Vdot

## 3.342014 [ft^3/s]
# given length of 1600 ft create a numeric vector with the units of feet
L_Eng <- set_units(1600, ft)
L_Eng

## 1600 [ft]
# create a numeric vector for gravity (US Customary units)
g_Eng <- set_units(9.80665 * (3937/1200), ft/sec^2)
g_Eng

## 32.17398 [ft/s^2]
# given saturated liquid density of oil (US Customary units)
rho_Eng <- set_units(1.75, slug/ft^3)
rho_Eng

## 1.75 [slug/ft^3]
# given kinematic viscosity of oil (US Customary units)
nu_Eng <- set_units(0.000115, ft^2/sec)
nu_Eng

## 0.000115 [ft^2/s]
# create a numeric vector with the units of feet for the given specific
# roughness
epsilon <- set_units(0.00085, ft)
epsilon

## 0.00085 [ft]
# create a numeric vector with the units of inch for the given internal pipe
# diameter
Di <- set_units(8, inch)
Di

## 8 [inch]
```



```

# create a numeric vector with the units of feet for the given internal pipe
# diameter
units(Di) <- make_units(ft)
Di

## 0.6666667 [ft]

# relative roughness (dimensionless) of the cast iron pipe
rel_roughness <- epsilon/Di
rel_roughness

## 0.001275 [1]

# internal area of the cast iron pipe
Ai <- Di^2 * pi/4
Ai

## 0.3490659 [ft^2]

# average velocity of the flowing water
V <- Vdot/Ai
V

## 9.574165 [ft/s]

# Reynolds number using the kinematic viscosity
Re_Eng <- Re2(D = drop_units(Di), V = drop_units(V), nu = drop_units(nu_Eng))
Re_Eng

## [1] 55502.41

# Darcy friction factor (f) for cast iron pipe Moody equation
fr2_Eng <- f2(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng)

# Romeo, et. al. equation
fr3_Eng <- f3(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng)

# Žarko Čojbašića and Dejan Brkić equation
fr4_Eng <- f4(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng)

# Colebrook-White equation
fr5_Eng <- f5(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng)

# Colebrook-White equation from Didier Clamond
colebrook_Eng <- colebrook(Re_Eng, K = drop_units(rel_roughness))

# Swamee-Jaine equation
fr6_Eng <- f6(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng)

# Zigrang-Sylvester equation
fr7_Eng <- f7(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng)

# Vatankhah equation
fr8_Eng <- f8(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng)

# friction loss for cast iron pipe
hf_Eng1 <- (f2(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng) * drop_units(L_Eng) *

```

```

drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_Eng))
hf_Eng2 <- (f3(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng) * drop_units(L_Eng) *
drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_Eng))
hf_Eng3 <- (f4(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng) * drop_units(L_Eng) *
drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_Eng))
hf_Eng4 <- (f5(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng) * drop_units(L_Eng) *
drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_Eng))
hf_Eng5 <- (colebrook(Re_Eng, K = drop_units(rel_roughness)) * drop_units(L_Eng) *
drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_Eng))
hf_Eng6 <- (f6(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng) * drop_units(L_Eng) *
drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_Eng))
hf_Eng7 <- (f7(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng) * drop_units(L_Eng) *
drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_Eng))
hf_Eng8 <- (f8(eps = drop_units(epsilon), D = drop_units(Di), Re = Re_Eng) * drop_units(L_Eng) *
drop_units(V)^2)/(2 * drop_units(Di) * drop_units(g_Eng))

# result table
result_table_Eng <- data.table(V1 = c("Moody equation", "Romeo, et. al. equation",
"Žarko Čojbašića and Dejan Brkić equation", "Colebrook-White equation",
"Colebrook-White equation from Didier Clamond", "Swamee-Jaine equation", "Zigrang-Sylvester equation",
"Vatankhah equation"), V2 = c(fr2_Eng, fr3_Eng, fr4_Eng, fr5_Eng, colebrook_Eng,
fr6_Eng, fr7_Eng, fr8_Eng), V3 = c(hf_Eng1, hf_Eng2, hf_Eng3, hf_Eng4, hf_Eng5,
hf_Eng6, hf_Eng7, hf_Eng8))

setnames(result_table_Eng, c("Darcy friction factor equation", "Darcy friction factor (f) for cast iron",
"Friction loss for cast iron pipe over total length"))

pander(result_table_Eng)

```

Darcy friction factor equation	Darcy friction factor (f) for cast iron pipe
Moody equation	0.02485
Romeo, et. al. equation	0.0224
Žarko Čojbašića and Dejan Brkić equation	0.02238
Colebrook-White equation	0.02444
Colebrook-White equation from Didier Clamond	0.02041
Swamee-Jaine equation	0.02464
Zigrang-Sylvester equation	0.02238
Vatankhah equation	0.02444

Friction loss for cast iron pipe over total length
84.94
76.59
76.52
83.57
69.79
84.25
76.52
83.54

R. Shankar Subramanian calculated 83.7 feet for the head loss.

## Works Cited

Charlie Young, P.E., EngineerExcel, “Colebrook Equation Solver in Excel”, <https://www.engineerexcel.com/colebrook-equation-solver-in-excel/>

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